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Pentachlorophenol removal from aqueous solutions by microwave/persulfate and microwave/H₂O₂: a comparative kinetic study

Ghorban Asgari¹, AbdolMotaleb Seidmohammadi¹ and Afsane Chavoshani^{2*}

Abstract

Pentachlorophenol (PCP) is one of the most fungicides and pesticides used in wood protection. Poisoning from PCP may be happened in dermal absorption, and respiration or ingestion. With regard to health and environmental effects of PCP, many methods were studied for its removal. Microwave assisted other methods are environmental friendly, safety, and economical method, therefore, in this study; a modified domestic microwave assisted hydrogen peroxide (MW/H₂O₂) and sodium persulfate (MW/SPS) was used for PCP removal from aqueous solutions. PCP removal rate was measured under different factors such as pH, energy intensity, SPS, H₂O₂ concentration, Tert- butyl alcohol (TBA) and chemical oxygen demand (COD). The concentration changes of PCP were determined using spectrophotometer and HPLC spectra, respectively. The best removal PCP rate obtained in condition of pH of 11, 0.02 mol L⁻¹ of SPS, 0.2 mol L⁻¹ of H₂O₂ and energy intensity of 600 W. Moreover, COD removals in MW/H₂O₂ and MW/SPS process were 83% and 94%, respectively, also TBA test decreased 15% and 3% of PCP removal in MW/SPS and MW/H₂O₂ processes respectively. Experimental results indicated that sulfate radical was stronger than hydroxyl radical and examinations order reaction was in first order. In this study, was cleared that MW/SPS process was more effective than MW/H₂O₂ process in PCP removal.

Keywords: Microwaves, Pentachlorophenol, Hydrogen peroxide, Sodium persulfate

Introduction

PCP, one of the phenolic compounds, is widely used in Wood protective industry [1]. Exposure of this compound makes diseases such as aplastic anemia, leukemia, peripheral neuropathy and other problems related to nerve damage (neurotoxicity). This pollutant is a significant contaminant of soil, surface, and groundwater especially around wood preserving facilities [2-6]. Researchers using a mathematical model calculated that 96.5% of PCP is in soil, 2.5% in water, 1% in air, and less than 1% in suspended sediments and organisms in aquatic environments [6,7]. Therefore, PCP removal from aqueous solutions is essential. According to previous studies is cleared that conventional treatment methods are ineffective for PCP and other refractory compounds removal, because these

methods can only transfer the contaminants from one phase to another producing many environmental problems [8]. Recently researchers have found that microwave (MW) heating in combination with hydrogen peroxide (H₂O₂) and sodium persulfate (Na₂S₂O₈ or SPS) [9] can mineralize organic compounds successfully and completely [6,10,11]. The key effects of these processes is the replacement of hazardous solvents with environmentally benevolent ones [8]. Basic of MW process is the ability of molecules or substances to absorb and transmit MW irradiation [12]. MW irradiation is electromagnetic irradiation in the frequency range of 0.3 to 300 GHz, but laboratory microwave reactors operate at frequency of 2.45 GHz [6,13,14]. By breaking oxygenoxygen bonds of $\rm H_2O_2$ and $\rm S_2O_8^{2-}$, MW commonly are able to dissociate $\rm H_2O_2$ and $\rm S_2O_8^{2-}$ into $\rm OH^0$ and $\rm SO_4^{0}$ radicals and other radicals which are very powerful oxidizing species [15].

Similar to hydroxyl radicals, sulphate radicals react with organics by electron transfer, hydrogen abstraction,

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or addition mechanisms [16,17]. According to results obtained of previous studies, SPS and $\rm H_2O_2$ could be a good option for the MW oxidation technique. In this study, due to an environmental-friendly in addition to highly efficient method and low existence of specific work in this condition, analysis of the PCP removal by MW/ $\rm H_2O_2$ and MW/SPS under various kinds of parameters was performed and in the end, the effectiveness of MW/SPS and MW/ $\rm H_2O_2$ processes in the PCP removal was compared.

Materials and methods

Materials

Sodium salt PCP, which is the sodium salt of PCP ($C_6C_{15}ONa$) with 98% purity was used without further purification. The characteristics of the PCP included of boiling point: 309-310 C^0 , mass molar: 288.32 g mol⁻¹. PCP solution was prepared by dissolving PCP in NaOH solution to accelerate its dissolution [6,18]. Hydrogen peroxide (30% w/w) and the sodium persulfate from Merck, 98% mass molar: 238.1 g mol⁻¹ were used as oxidants.

Experimental methods and measurements

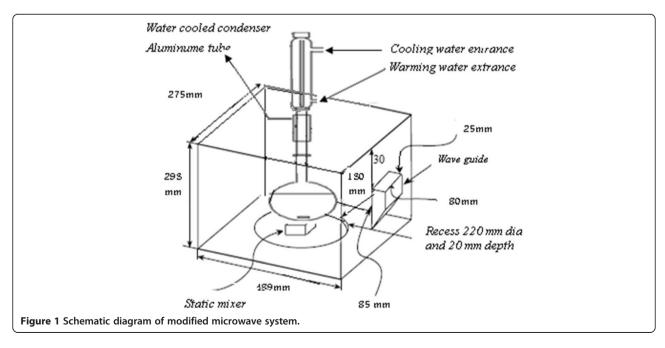
Under atmospheric pressure, all of the experiments were performed and triplicated in modified domestic microwave oven (2450 MHz, M2330 DN, SAMSUNG Co, and output power of 100 to 850 W) (Figure 1). Detail modifications of MW were presented as follows: drilled a hole in the upper oven wall and then attached an aluminum tube of the same diameter to the hole then equipped with cooling system and a glass reactor with 500 mL volume. Then Samples were taken at

suitable time intervals (10 min) from the reaction reactor with a 10 mL syringe and pipetted in to glass vials [6,11]. Besides, a Thermometer GENWAY Medal 2003 was utilized to detect variation of solution temperature during degradation process. The leakage of MW oven is measured at 20 cm distance from the aperture.

In this study different factors effects such as pH (3, 7, 11), energy intensity (180,450,600 W with optimal temperatures 80, 100, and 105C⁰ respectively), SPS and H_2O_2 dose (0.01, 0.02, 0.03, 0.04, 0.05 mol L⁻¹), PCP concentration (100, 200, 300, 400, 500, 750, 1000 mg L⁻¹), effect of Tert-butyl alcohol (TBA) with 0.04 mol L⁻¹ concentration, and COD (344 mg L⁻¹) were determined. Changes of PCP concentration were detected using spectrophotometer according to (APHA [19]), and HPLC. HPLC (Part Number.WATO54275 with dimension of 4.6 mm × 250 mm and column of symmetry C18-50 µm) method was performed with an acetonitrile/water 60:40 (v/v) as mobile phase at a flow rate of 1 mL min⁻¹ and detection wavelengths of UV was 254 nm [6,20]. COD was detected using potassium dichromate solution as oxidizer in a strong acid medium, then by titration step using ferrous ammonium sulfate as the reducing agent and Ferroin as the indicator [6,9].

Results and discussion Effect of pH on PCP removal

In this study under MW/SPS and pHs of 3,7and 11, PCP removal rate was 48, 56, 67% respectively, but under MW/ H_2O_2 , its amount was 42, 53 and 56% respectively (Figure 2). It seems that strong power of MW in ionization of SPS and H_2O_2 leads to a negligible difference between



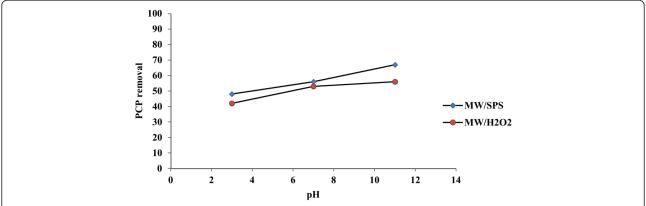


Figure 2 Effect of pH on PCP removal under MW/SPS and MW/ H_2O_2 systems (PCP = 100 mg L^{-1} , E = 600W, SPS and H_2O_2 dose = 0.02 mol L^{-1} , reaction time = 30 min).

all pHs effect (Figure 2), therefore more research for pH effect is necessary. However, results shown that alkaline pH could more accelerate PCP degradation in MW/SPS and MW/ H_2O_2 systems. These phenomena under MW/SPS and MW/ H_2O_2 were attributed to the ability of H_2O_2 and SPS to absorb and transmit microwave irradiation in alkaline pH more a little than other pHs. Subsequently more radicals are produced in this condition [21-25].

In general and according to experimental conditions following reactions can be performed:

Under MW/SPS:

All pHs:
$$SO_4^{0-} + H_2O \rightarrow SO_4^{-2} + OH^0 + H^+$$
 (1)

Alkaline pH:
$$SO_4^{0-} + OH^- \rightarrow SO_4^{-2} + OH^0$$
 (2)

Under MW/H₂O₂:

$$H_2O_2 + MW \rightarrow 2OH^0 \tag{3}$$

$$OH^0 + H_2O_2 \rightarrow H_2O + HO_2^0$$
 (4)

$$2OH^0 \rightarrow H_2O_2 \tag{5}$$

$$2OH^0 \rightarrow H_2O_2 + O_2 \tag{6}$$

$$OH^0 \leftrightarrow O_2^- + H^+ \tag{7}$$

$$H_2O + HO_2^0 + O_2^- \rightarrow H_2O_2 + O_2 + OH$$
 (8)

Under MW/SPS, the rate constants for Eqs. (1) and (2) are $< 2 \times 10^{-3}$ and $(6.5 \pm 1) \times 10^7$ M $^{-1}$ S $^{-1}$ respectively. It is cleared that the reaction rate constant of Eq. (2) is more than Eq. (1). According these equations in all pHs and alkaline pH, both $SO_4^{\ 0-}$ and OH^0 are possibility responsible for degradation of organic contaminants, but previous studies have shown that in pHs of 3–10, amount of hydroxyl radical is more than sulfate radical and in pH > 10.5 amount of sulfate radical is more than hydroxyl [26,27]. According these results, the difference

between our work and previous studies could partly attribute to pH = 11. Results of other studies confirm that organic removal efficiency is more in alkaline pH [15]. In similar to, under MW/H_2O_2 in alkaline pH, amount of OH^0 and other radicals participating in PCP removal is more than other pHs (Eqs (3) to (8)) [6,11,28].

Effect of SPS and H₂O₂ concentrations on PCP removal

From Figure 3 is observed that under MW/SPS with increasing SPS concentration from 0.01 to 0.0 2 mol L $^{-1}$, PCP removal efficiency was increased (56 to 94%). But with increasing the initial SPS concentration from 0.02 to 0.05 mol L $^{-1}$ PCP removal rate was decreased from 94 to 49% respectively. Furthermore under MW/H $_2$ O $_2$, PCP removal efficiency for 0.01 to 0.05 mol L $^{-1}$ of H $_2$ O $_2$ was 12.5% to 75% respectively. PCP removal (87%) was stabled in doses of 0.2 and 0.3 mol L $^{-1}$ of H $_2$ O $_2$ (data not show). Therefore, optimal doses of SPS and H $_2$ O $_2$ were 0.02 and 0.2 mol L $^{-1}$ respectively. Shih et al. reported that, in extremely high initial concentration, SO $_4$ 0 $^-$ 1 reacted with persulfate according to the following equation [29].

$$SO_4^{0-} + S_2O_8^{2-} \rightarrow SO_4^{2-} + S_2O_8^{0-}$$
 (9)

So that an over-dose of persulfate transformed the $SO_4^{\ 0^-}$ to $S_2O_8^{\ 0^-}$ reducing the oxidizing power for PCP removal [30,31]. Also with respect to Eq (10), under high H_2O_2 concentration in MW/H_2O_2 system, quenching of OH° radicals is happened to produce HO_2° radicals [6,11,15].

$$H_2O_2 + OH^0 \rightarrow H_2O + HO_2^0$$
 (10)

Therefore, existences of a scavenger of OH° radicals, such as H_2O_2 , have a decreasing effect in the organic compounds removal efficiency [6,17].

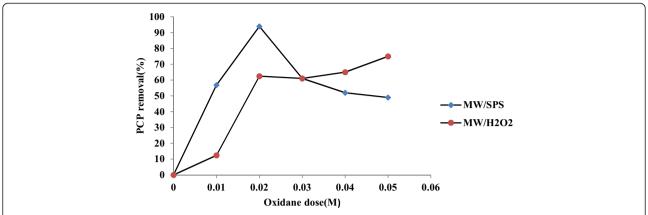


Figure 3 Effect of oxidant concentration on PCP removal under MW/SPS and MW/ H_2O_2 systems (pH = 11, PCP = 100 mg L^{-1} , E = 600 W, reaction time = 30 min).

Effect of different energy intensity on PCP removal

The test results shown in Figure 4 indicated that PCP removal efficiency gradually increased by increasing the microwave power from 180 to 600 W. Amount of PCP removal in MW/SPS with energy intensity of 180, 450, and 600 W was 26, 89 and 93%, respectively. In addition, under MW/H₂O₂ system amount of PCP removal was 20, 80 and 87%, respectively. PCP removal efficiency did not change for higher power (>600 W). Subsequently, the microwave irradiation of 600 W was chosen for further experiments. According to other studies, removal efficiency can only increase to a limited extent [32] and degradation of organic materials is not always increased with increasing microwave power [33,34]. In this study, amount of Energy consumption in optimal condition

(energy power of 600 W and reaction time of 30 min) for both of systems was 0.3 KWh, also other researchers confirm that energy consumption in MW process is very low and economy [35,36].

Effect of radical scavenger on PCP removal

In this study, 0.04 mol L $^{-1}$ TBA (OH 0 scavenger) added to MW/SPS and MW/H $_{2}$ O $_{2}$. The results shown that the degradation rate of PCP was decreased 15% and 3% under MW/SPS/TBA and MW/H $_{2}$ O $_{2}$ /TBA respectively (Figure 5). According to Eqs. (11) to (16) [37] is cleared that both SO4 $^{0-}$ and OH 0 can degrade PCP, but with respect to TBA test, SO $_{4}^{0-}$ in MW/SPS play the dominant role and OH 0 had only a negligible role (15%).

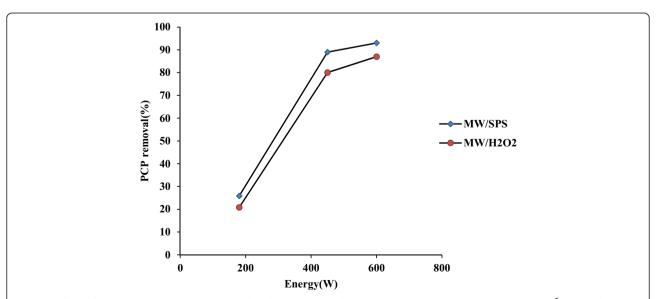


Figure 4 Effect of energy intensity on PCP removal under MW/SPS and MW/ H_2O_2 systems (pH = 11, PCP = 100 mg L^{-1} , SPS and H_2O_2 dose = 0.02 and 0.2 mol L^{-1} , reaction time = 30 min).

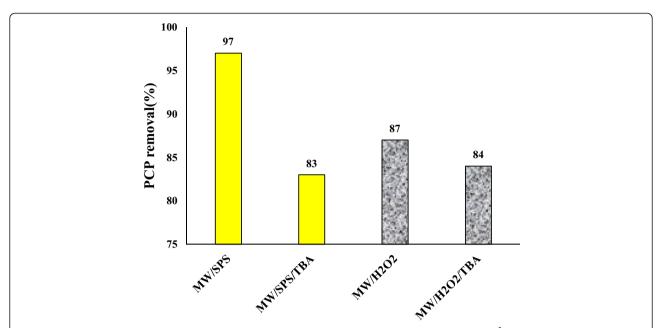


Figure 5 Effect of TBA on PCP removal under MW/SPS and MW/H $_2$ O $_2$ systems (pH = 11, PCP = 100mg L $^{-1}$, SPS and H $_2$ O $_2$ dose = 0.02, 0.2 mol L $^{-1}$, TBA = 0.04 mol L $^{-1}$, E = 600 W, reaction time = 30 min).

(12)

(14)

$$-O_3S-O-O-S-O_3 \to 2-O_3S-O_3$$

(11)
$$OH^0 + PCP \rightarrow Products$$
 (16)

$$-O_3S-O^0 + e^- \rightarrow SO_2^{-4}$$

$$-O_3S-O^0 + PCP \rightarrow Products$$
 (13)

$$- O_3 S - O^0 + H_2 O {\longrightarrow} HSO^{-4} + OH^0$$

$$-O_3S-O^0 + HO^- \rightarrow SO_2^{-4} + OH^0$$

$$MW/H_2O_2/TBA$$
 results show that OH^0 is activation initiator and isn't dominant radical (its role was only 3%). Based on following equations, MW is able to dissociate H_2O_2 to many radicals as well as OH^0 [6,28,38].

Also according to Hong et al. results in MW/H_2O_2 system, O_2 is dominant radical [9].

(15)
$$H_2O_2 + MW \rightarrow 2OH^0$$
 (17)

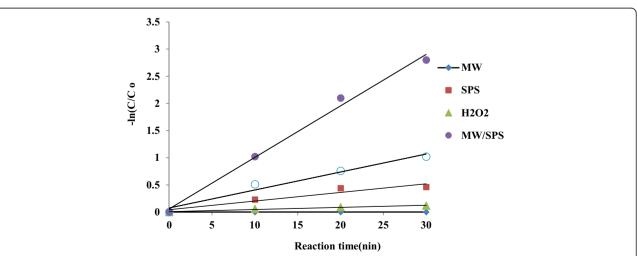


Figure 6 Reaction kinetics of PCP removal under different processes (pH = 11, PCP = 100 mg L^{-1} , SPS, H_2O_2 dose = 0.02, 0.2 mol L^{-1} , E = 600 W, reaction time = 30 min).

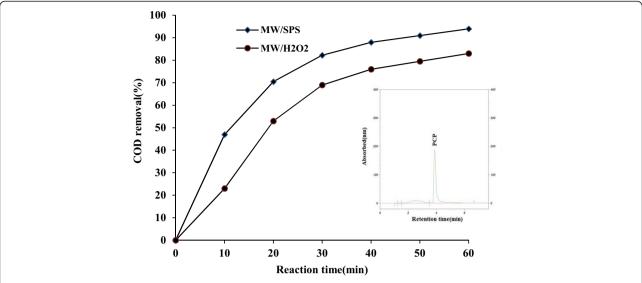


Figure 7 Mineralization of PCP in MW/SPS and MW/ H_2O_2 processes and identification of oxidation intermediates (pH = 11, COD = 344 mg/L, SPS and H_2O_2 dose = 0.02 and 0.2 mol L^{-1} , E = 600 W).

$$OH^0 + H_2O_2 \rightarrow H_2O + HO_2^0$$
 (18)

$$2OH^0 \rightarrow H_2O_2 \tag{19}$$

$$2OH^0 \rightarrow H_2O_2 + O_2$$
 (20)

$$OH^0 \leftrightarrow O_2^- + H^+ \tag{21}$$

$$H_2O + HO_2^0 + O_2^- \rightarrow H_2O_2 + O_2 + OH^-$$
 (22)

Reaction kinetics

Obtained Results from reaction kinetics under MW/SPS and MW/H₂O₂ demonstrated that the PCP removal follows first-order kinetics law (Figure 6). In this study, K SPS and K $\rm H_2O_2$ only was 0.014 min⁻¹ and 0.004 min⁻¹ respectively, but K MW/SPS and K MW/H₂O₂ was 0.095 min⁻¹ and 0.055 min⁻¹ respectively. So that, K SPS was 3.5 times more than K $\rm H_2O_2$, and K MW/SPS was 1.72 times more than K MW/H₂O₂. Because energy of oxygen-oxygen bond in persulfate is less than $\rm H_2O_2$ [15], SPS activation and subsequently PCP removal occur more rapidly in MW/SPS system than MW/H₂O₂. Also synergetic factor of MW in MW/SPS and MW/H₂O₂ was 6.6 and 13.75 respectively. This factor shows that MW process have higher synergetic effect on $\rm H_2O_2$ decomposition than SPS [39].

Mineralization of PCP in MW/SPS and MW/H₂O₂ processes and identification of oxidation intermediates

Results abstained from COD removal showed that MW/SPS and MW/ $\rm H_2O_2$ were able to remove COD in amount of 94 and 83% respectively (Figure 7). Intermediates detected via HPLC were $\rm CO_2$ and HCL (Eq. 23). In this

study, the HPLC spectra and COD results showed a similar trend in mineralization and the lack of toxic intermediates and by products [28,39].

$$C_6HCL_5O + MW \rightarrow CO_2 + 5HCl$$
 (23)

Conclusion

MW/SPS and MW/H₂O₂ processes could efficiently degrade refractory compounds at strong alkaline, via radical production. MW/SPS in PCP removal was more effective than MW/H2O2, because SPS is dissociated and activated more easily than hydrogen peroxide. Addition of SPS and H₂O₂ doses during MW process enhances the rate of PCP degradation, except when the radical scavenging effects of SPS and H₂O₂. Results obtained from radical scavenger test showed that OH° had only an initiator role, and had not a dominant role and order reaction in both of systems was in first order. Also, the microwave degradation is able to mineralize refractory compounds without any toxic byproduct. The microwave degradation has many advantages such as convenience, safety, economy and high efficiency. Accordingly these methods, especially WM/SPS, have a better prospect in future for removal of other chlorinated organic compounds such as Aldrin, Dieldrin and Lindane, in alkaline pH.

Abbreviations

PCP: Pentachlorophenol; AOPs: Advanced oxidation processes; TBA: Tert- butyl alcohol; COD: Chemical oxygen demand; SPS: Sodium Persulfate; H_2O_2 : Hydrogen Peroxide; MW: Microwave; K: Reaction constant.

Competing interests

The authors declare that they have no competing interests.

Authors' contributions

All authors studied and approved the final manuscript.

Acknowledgements

The authors would like to thank Hamadan University of Medical Sciences for technical and financial support of this work (9010274023).

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Received: 21 November 2013 Accepted: 5 May 2014 Published: 11 June 2014

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doi:10.1186/2052-336X-12-94

Cite this article as: Asgari et al.: Pentachlorophenol removal from aqueous solutions by microwave/persulfate and microwave/H₂O₂: a comparative kinetic study. *Journal of Environmental Health Science & Engineering* 2014 12:94.